

FIG. 1 is a schematic diagram of a device for the electrolysis of water.

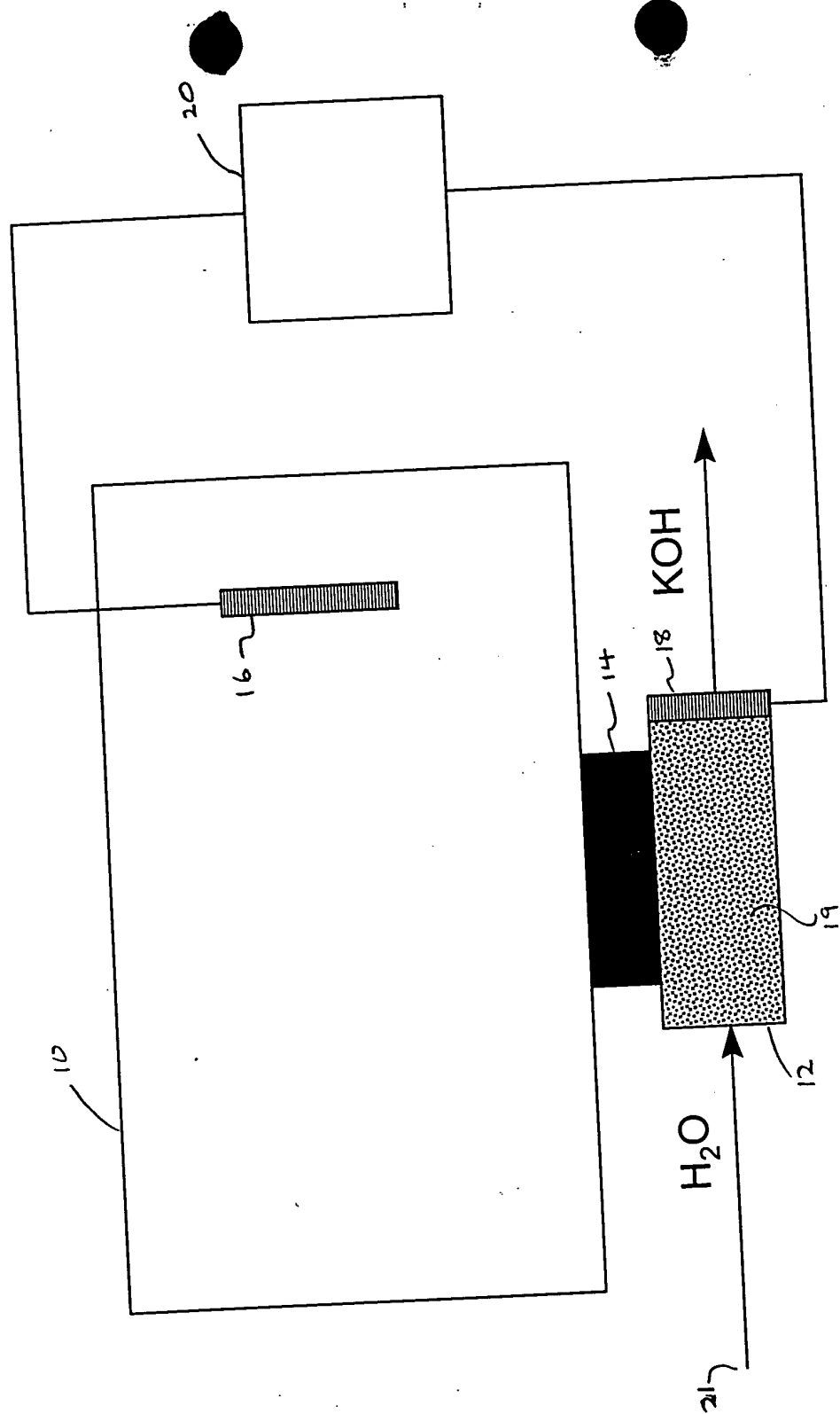


Figure 1.

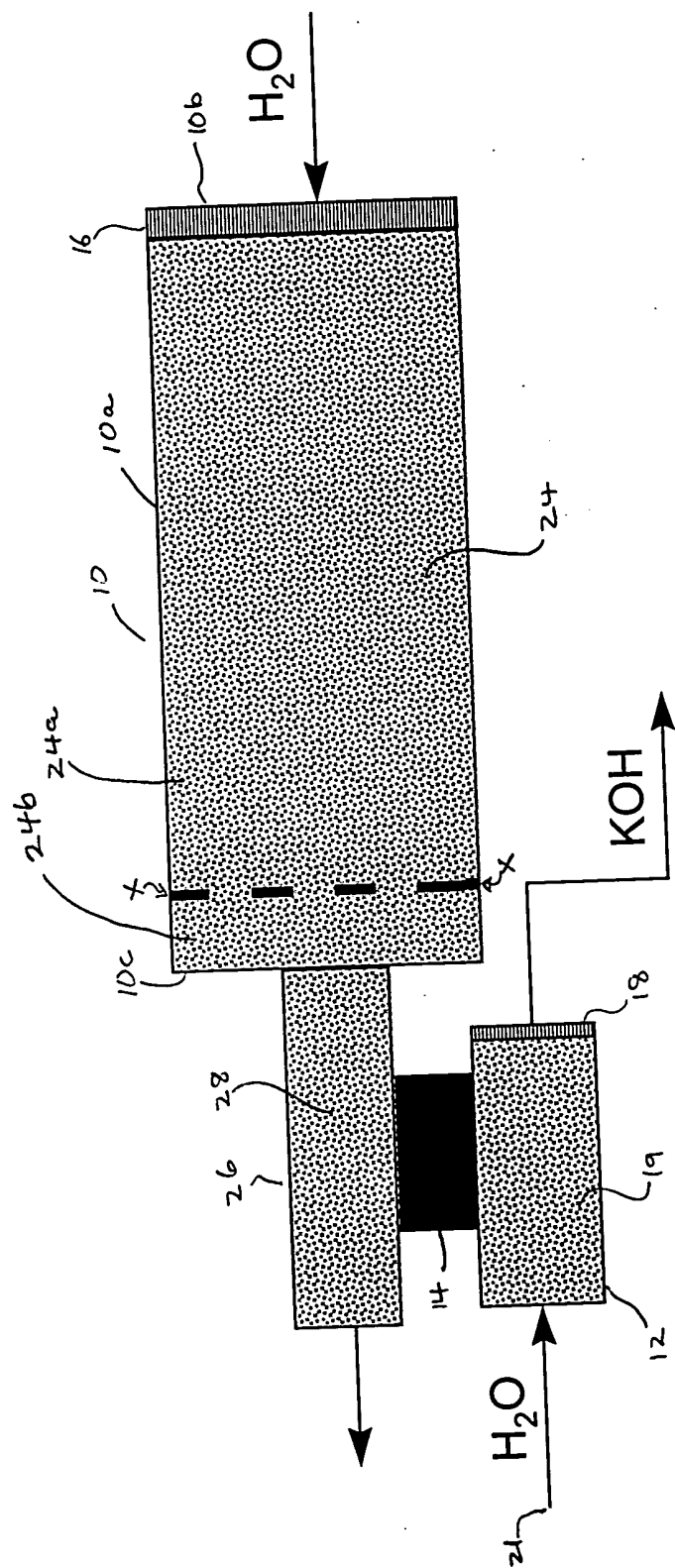


Figure 2.

FIG. 3 is a schematic diagram of a system for the production of hydrogen gas. The system includes a water supply (12) which feeds into a reactor (14) containing a catalyst (16). The reactor is connected to a gas collection system (18) which produces hydrogen gas (H₂O). The gas collection system is connected to a storage tank (20) which stores the hydrogen gas. The storage tank is connected to a delivery system (22) which delivers the hydrogen gas to a user.

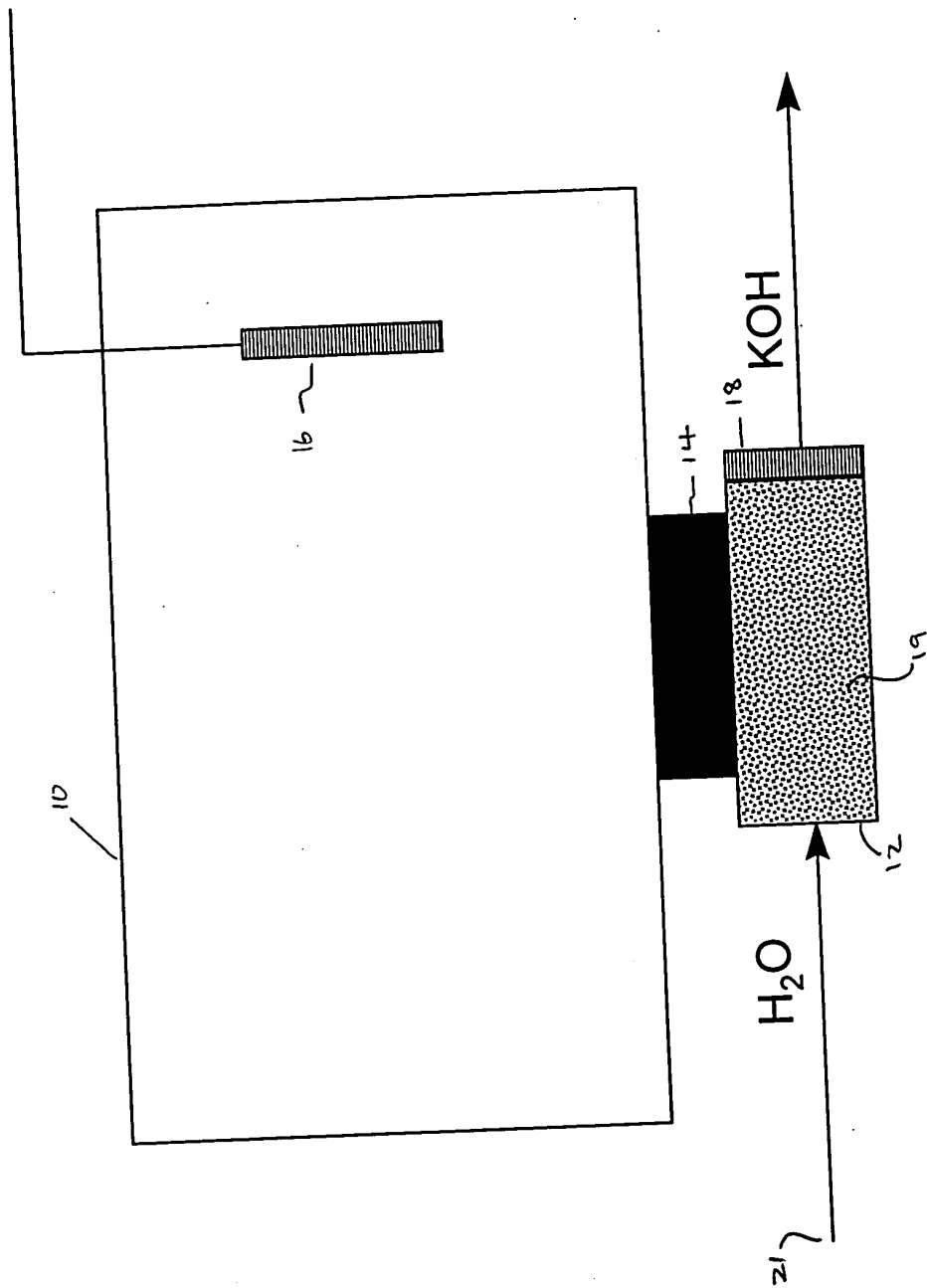


Figure 3.

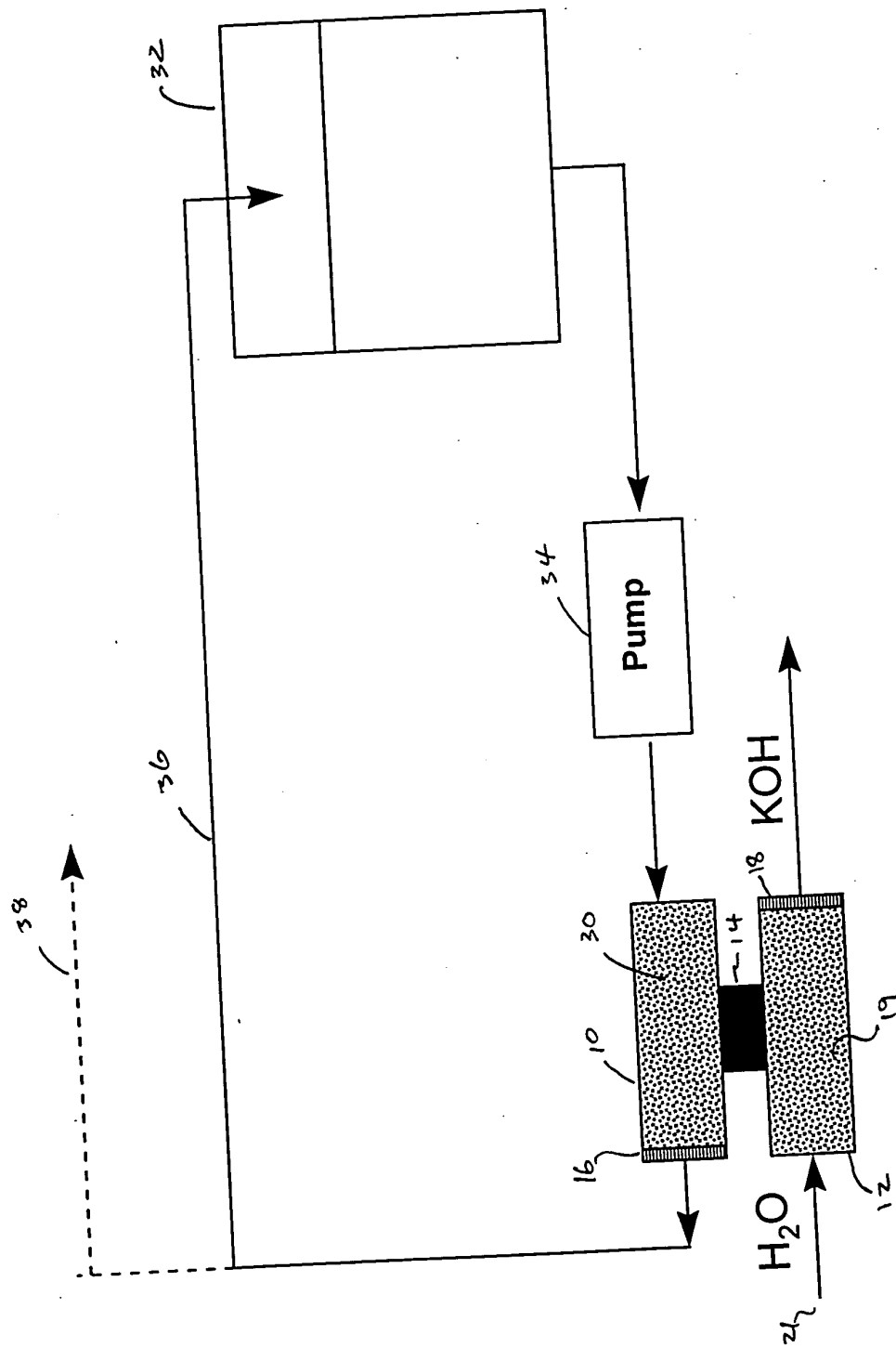


Figure 4.

The diagram illustrates a three-stage electrochemical process for producing hydrogen peroxide. The system, labeled 10, consists of three electrolytic cells (12a, 12b, 12c) connected in series. Each cell contains an anode (18a, 18b, 18c) and a cathode (19). The cells are separated by dividers (14a, 14b, 14c). The first cell (12a) receives H₂O and produces H₂. The second cell (12b) receives H₂ and produces H₂O₂. The third cell (12c) receives H₂O₂ and produces KOH. A power source (16) is connected to the anodes of the first and third cells. The entire system is labeled 10.

Figure 5.

FIG. 6 is a schematic diagram of a fuel cell system. The system includes a fuel cell 10, a water inlet 12, a water outlet 14, a KOH inlet 16, and a KOH outlet 18. The fuel cell 10 is connected to a power source 20. The water inlet 12 is connected to a water reservoir 22. The water outlet 14 is connected to a water reservoir 24. The KOH inlet 16 is connected to a KOH reservoir 26. The KOH outlet 18 is connected to a KOH reservoir 28.

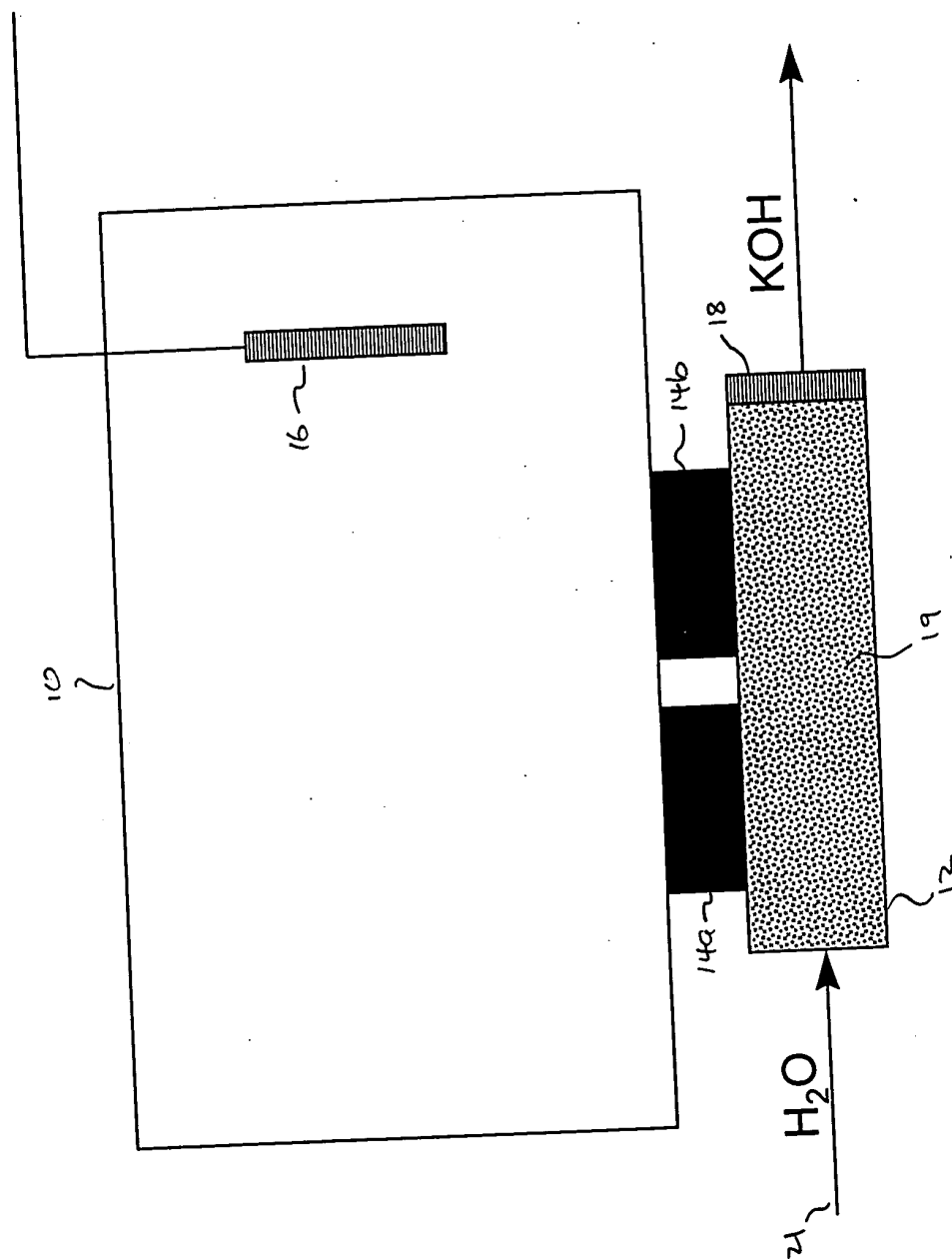


Figure 6.

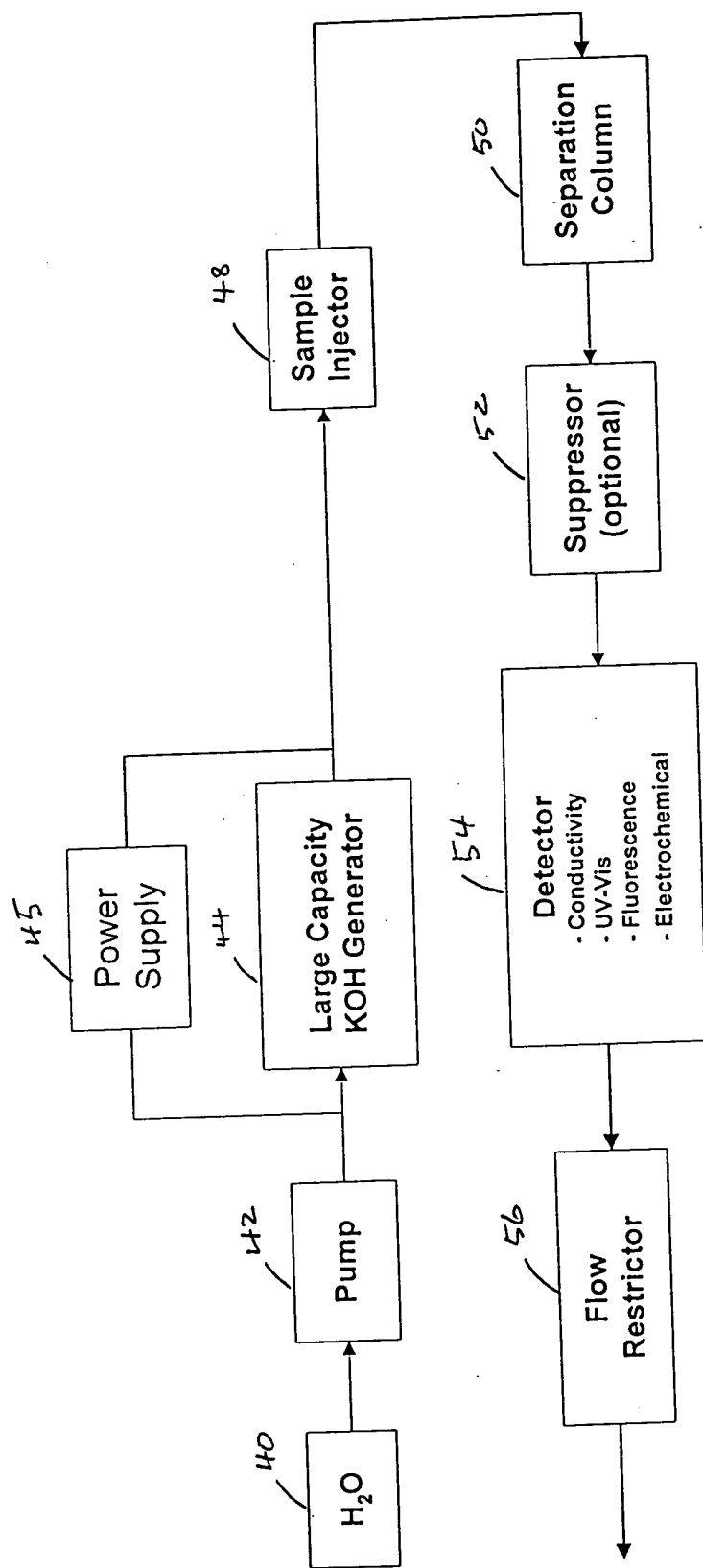


Figure 7.

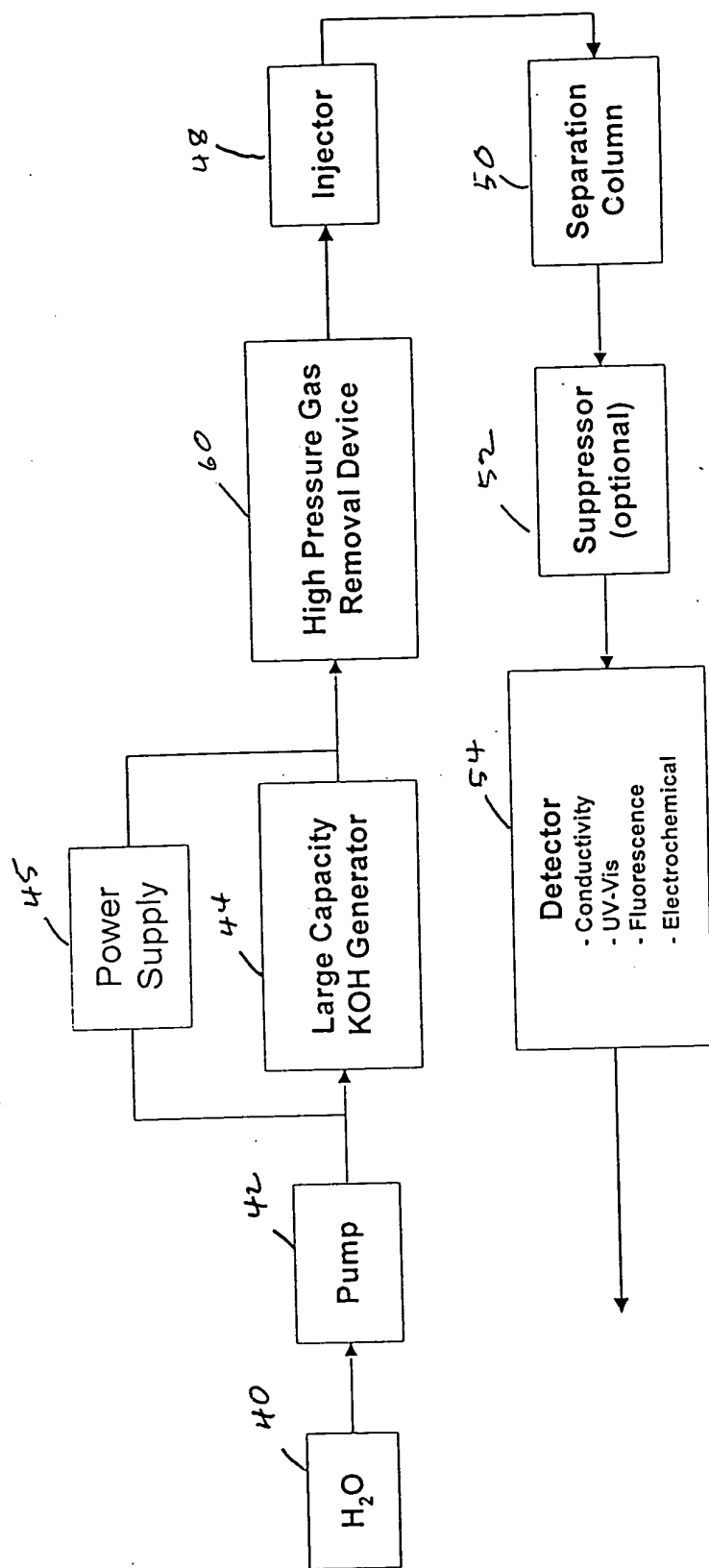


Figure 8.

Figure 9 is a schematic diagram of a chemical process. The diagram shows a horizontal rectangular vessel with an internal partition. On the left side, an inlet stream labeled $\text{KOH} + \text{H}_2$ enters through a line labeled 62. On the right side, an outlet stream labeled KOH exits through a line labeled 64. A third stream, labeled 67, exits from the top of the vessel. The internal partition is labeled 66.

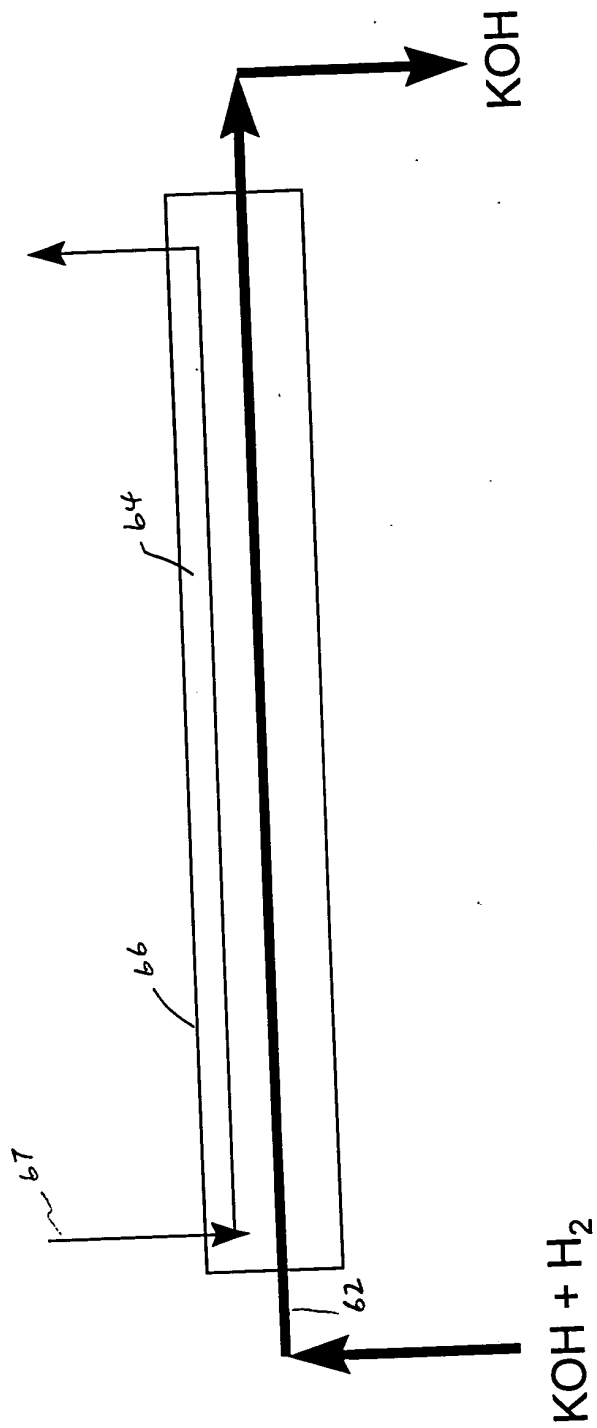


Figure 9.

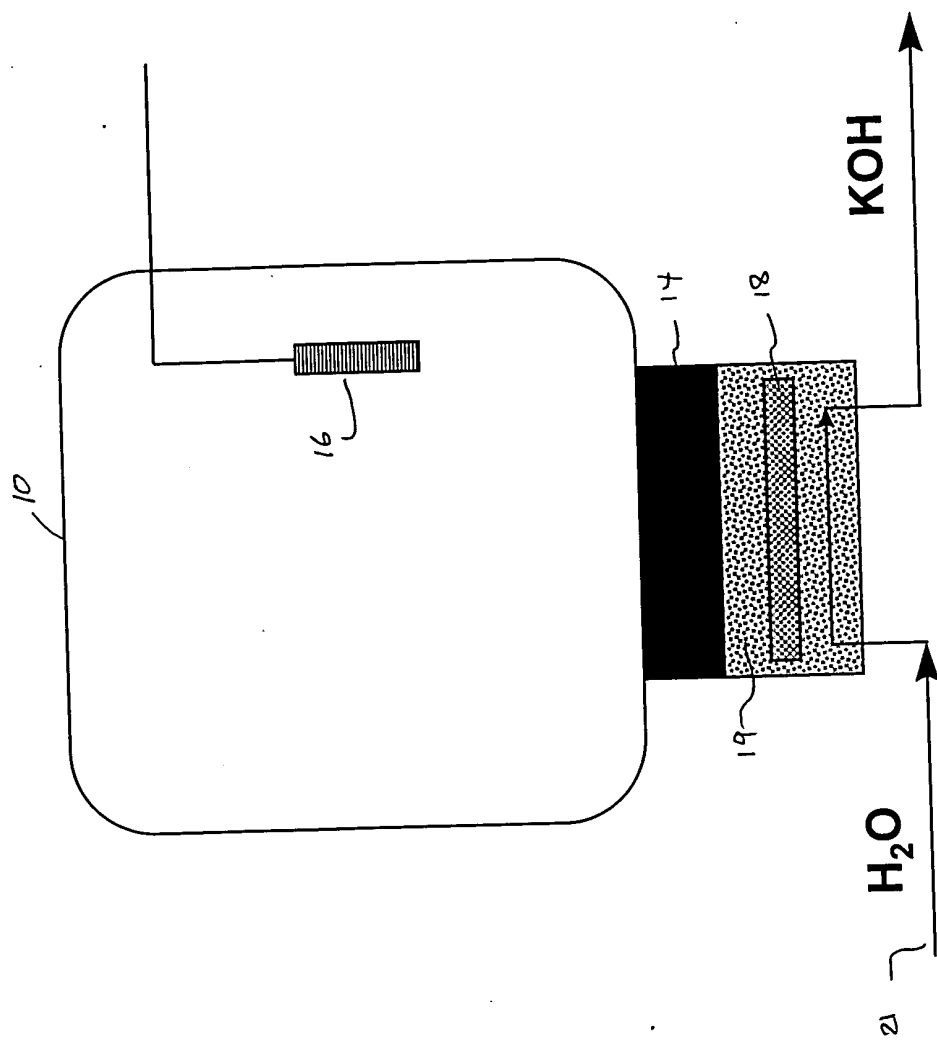


Figure 10.

FIG. 11 is a schematic diagram of a fuel cell system.

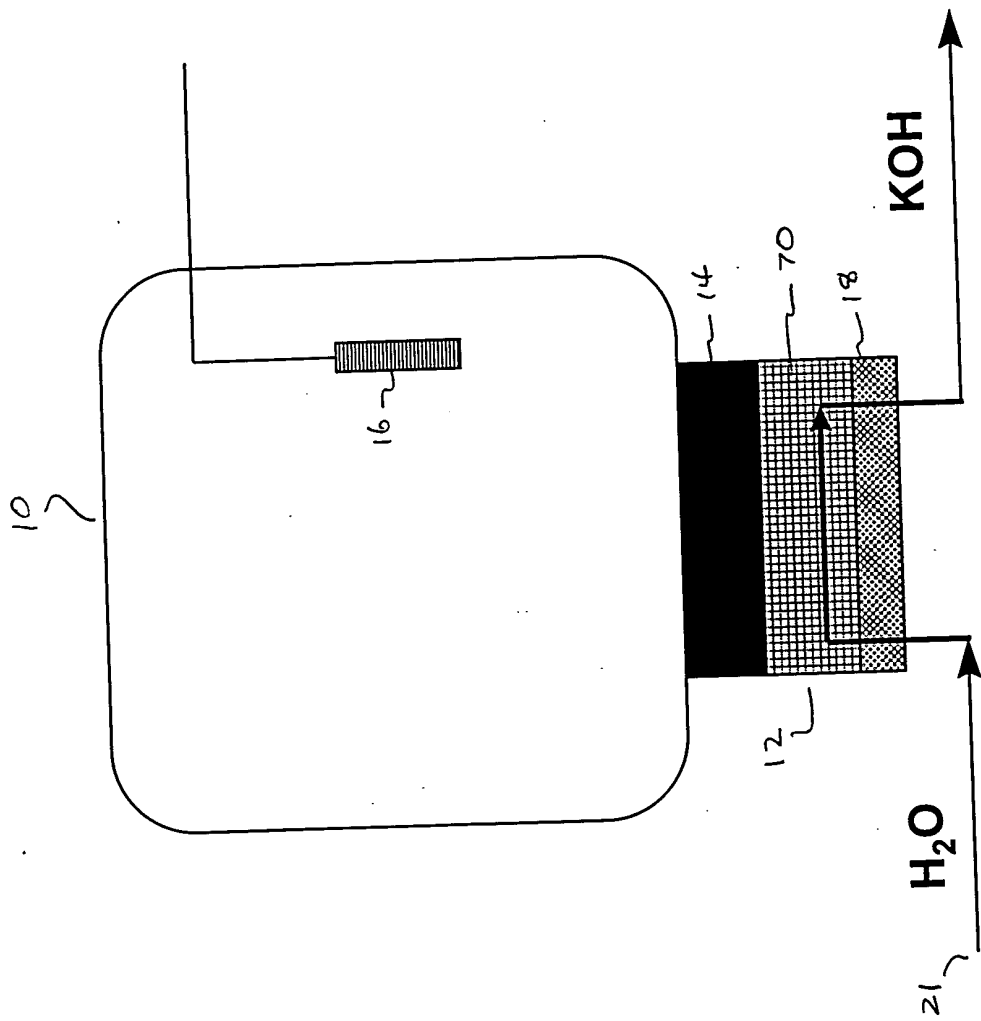


Figure 11.

any other of the above described systems may be used in the present invention.

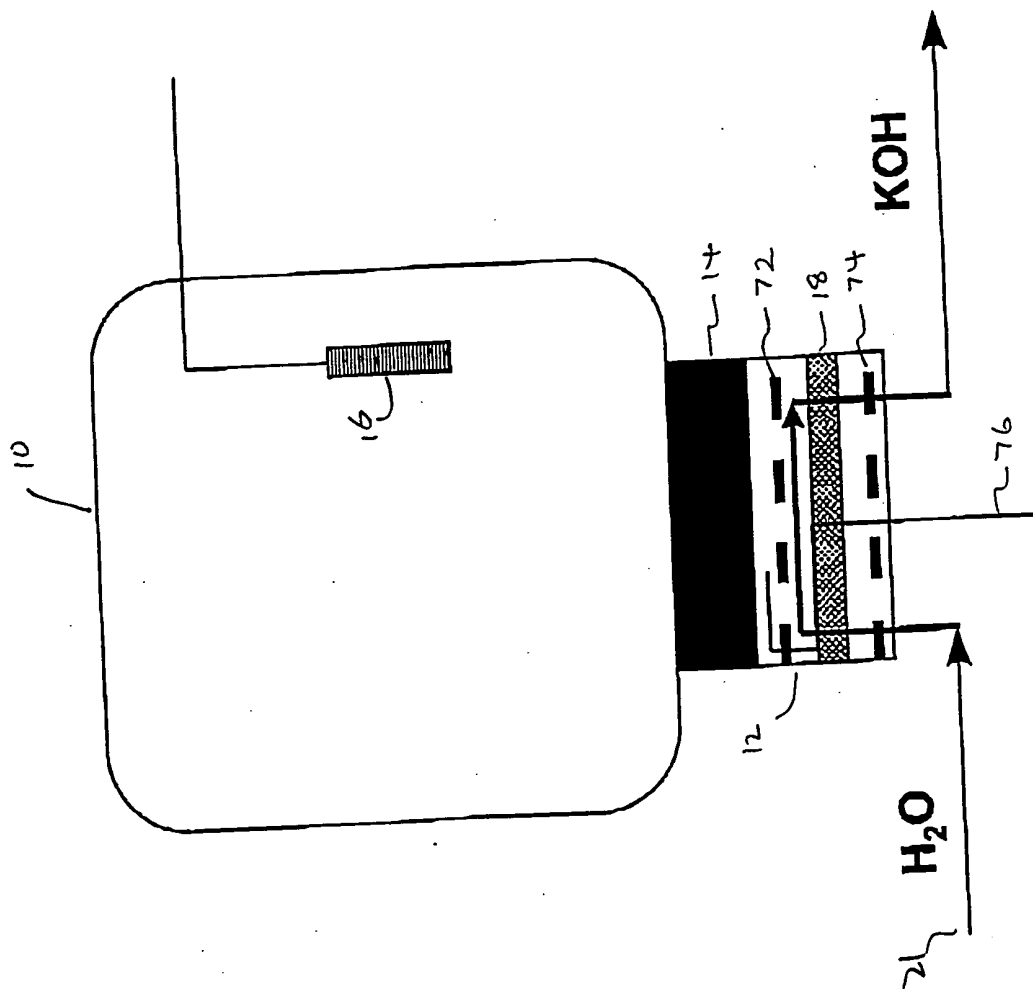


Figure 12.

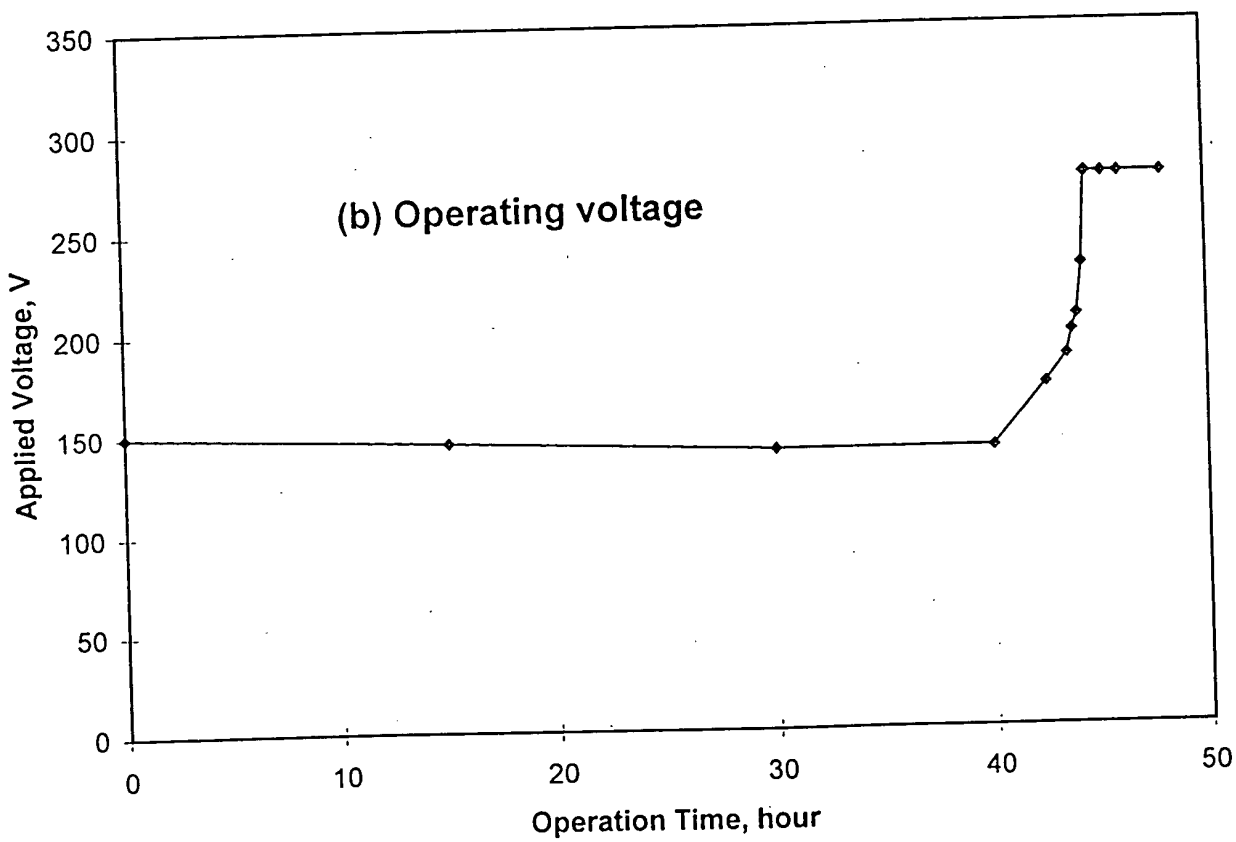
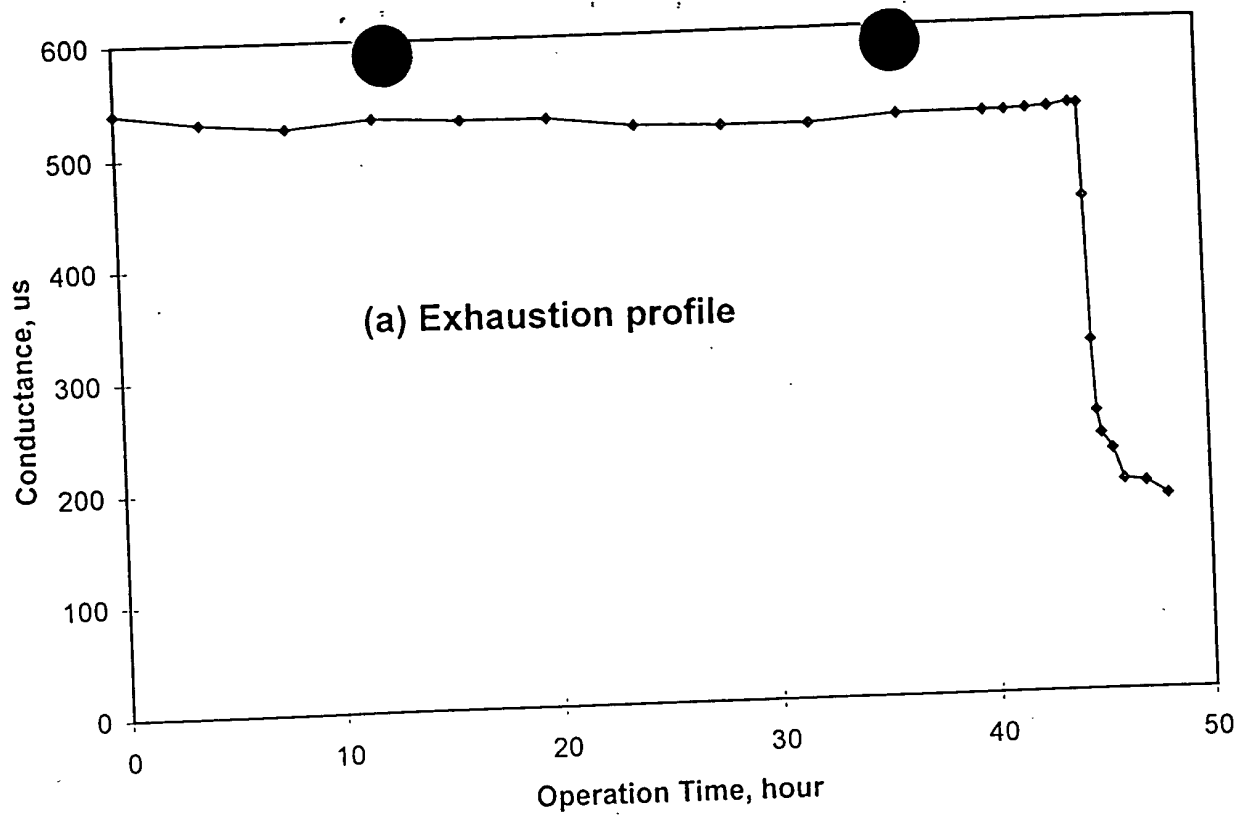


Figure 13.

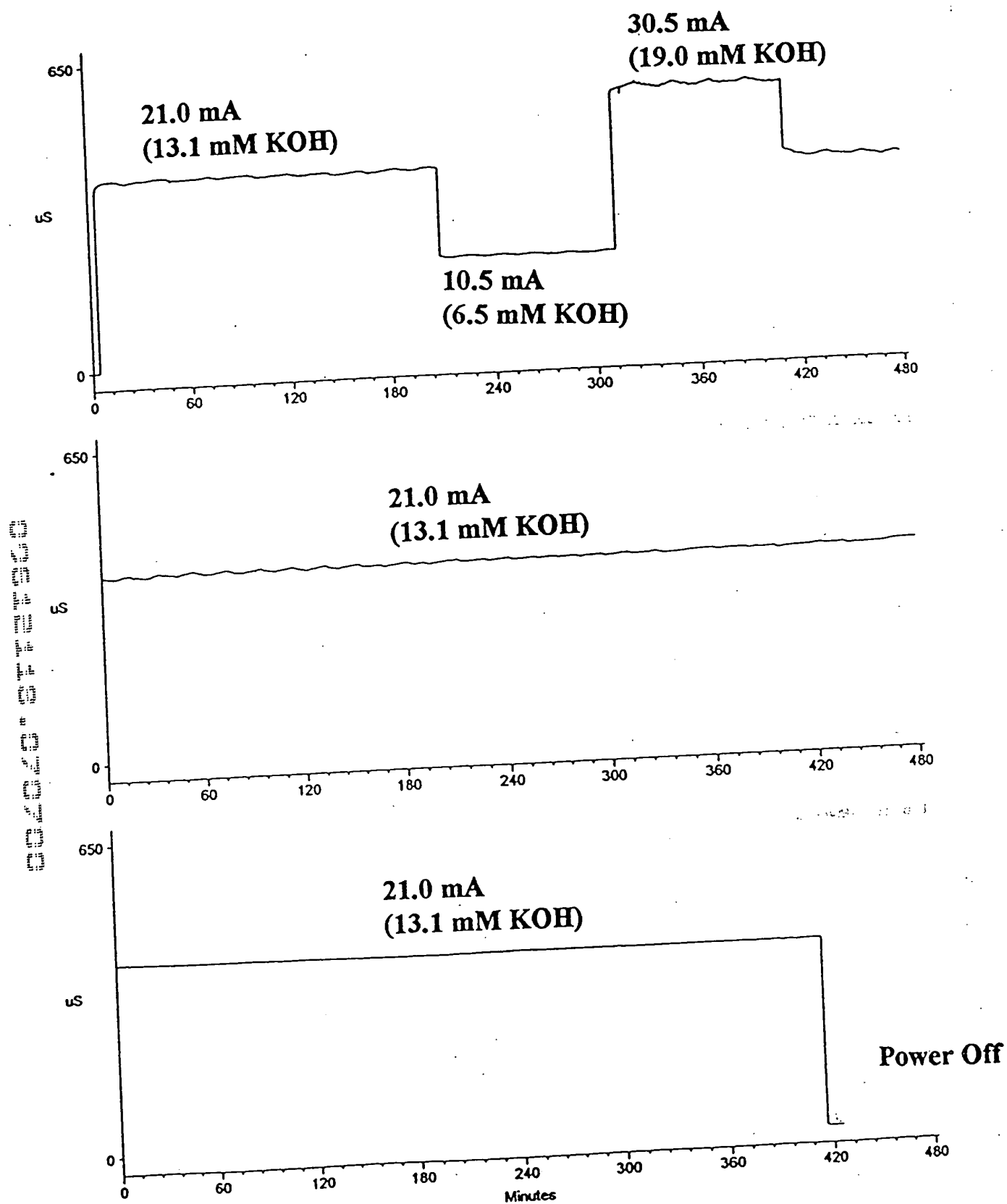


Figure 14.

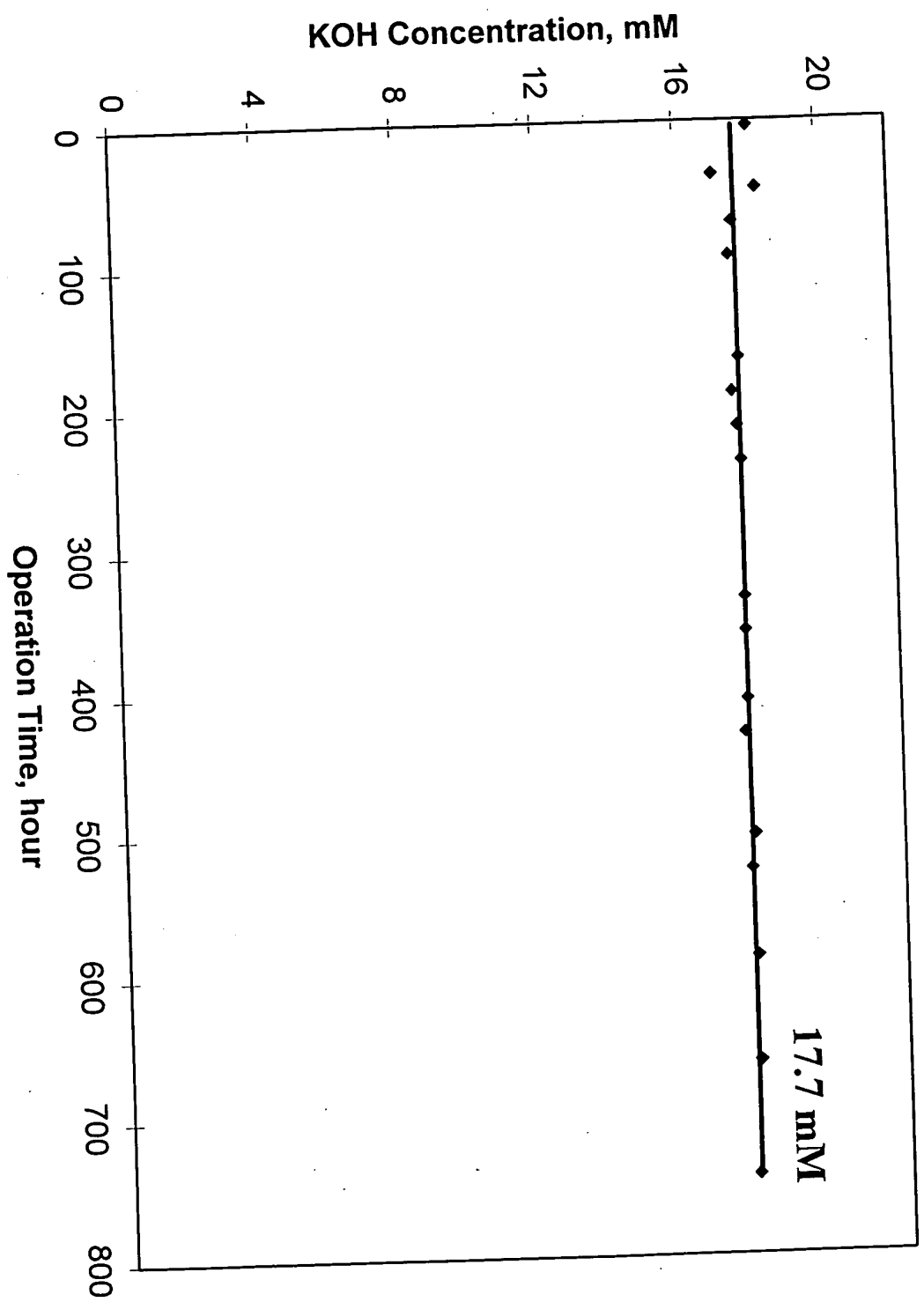


Figure 15.

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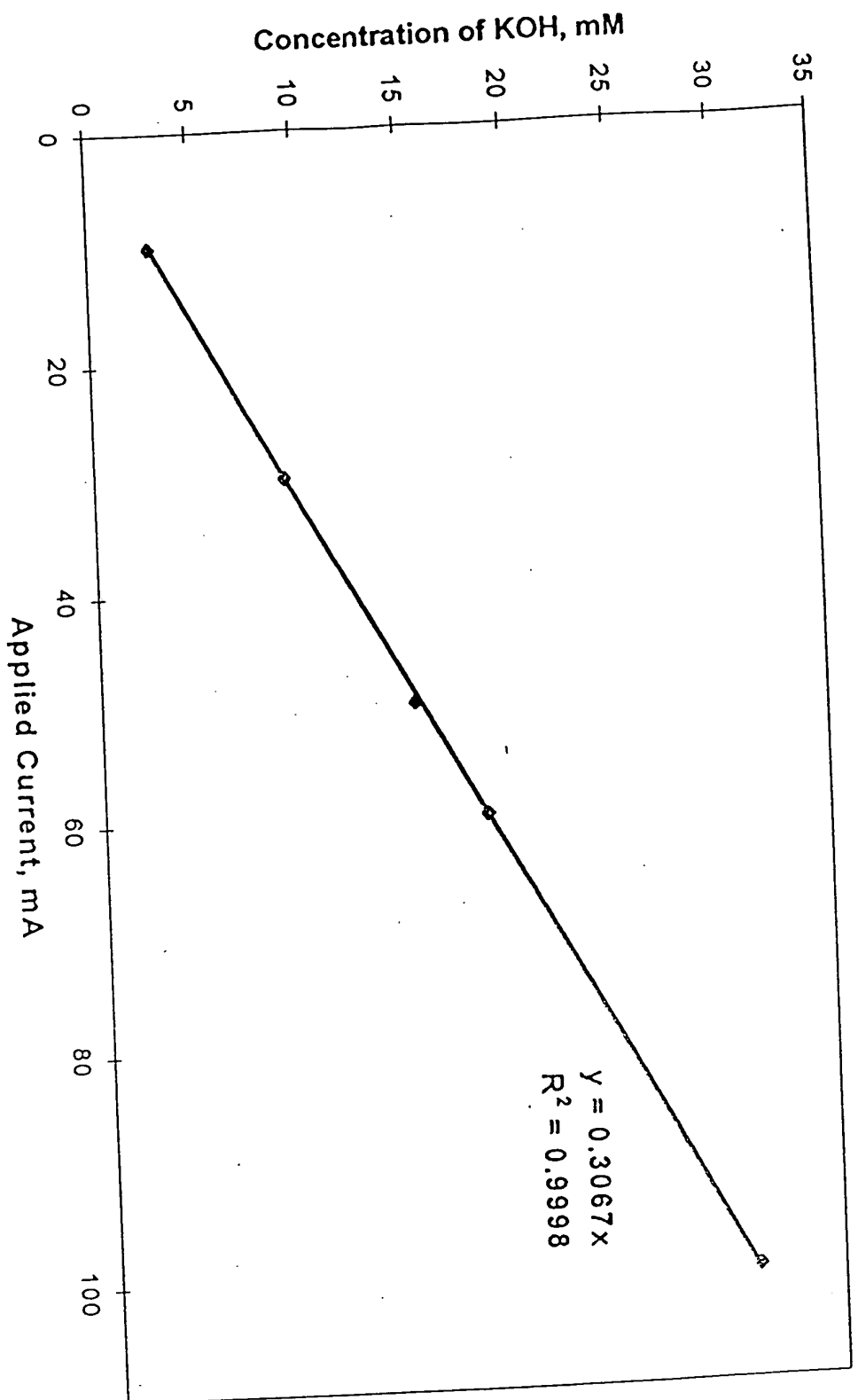


Figure 16

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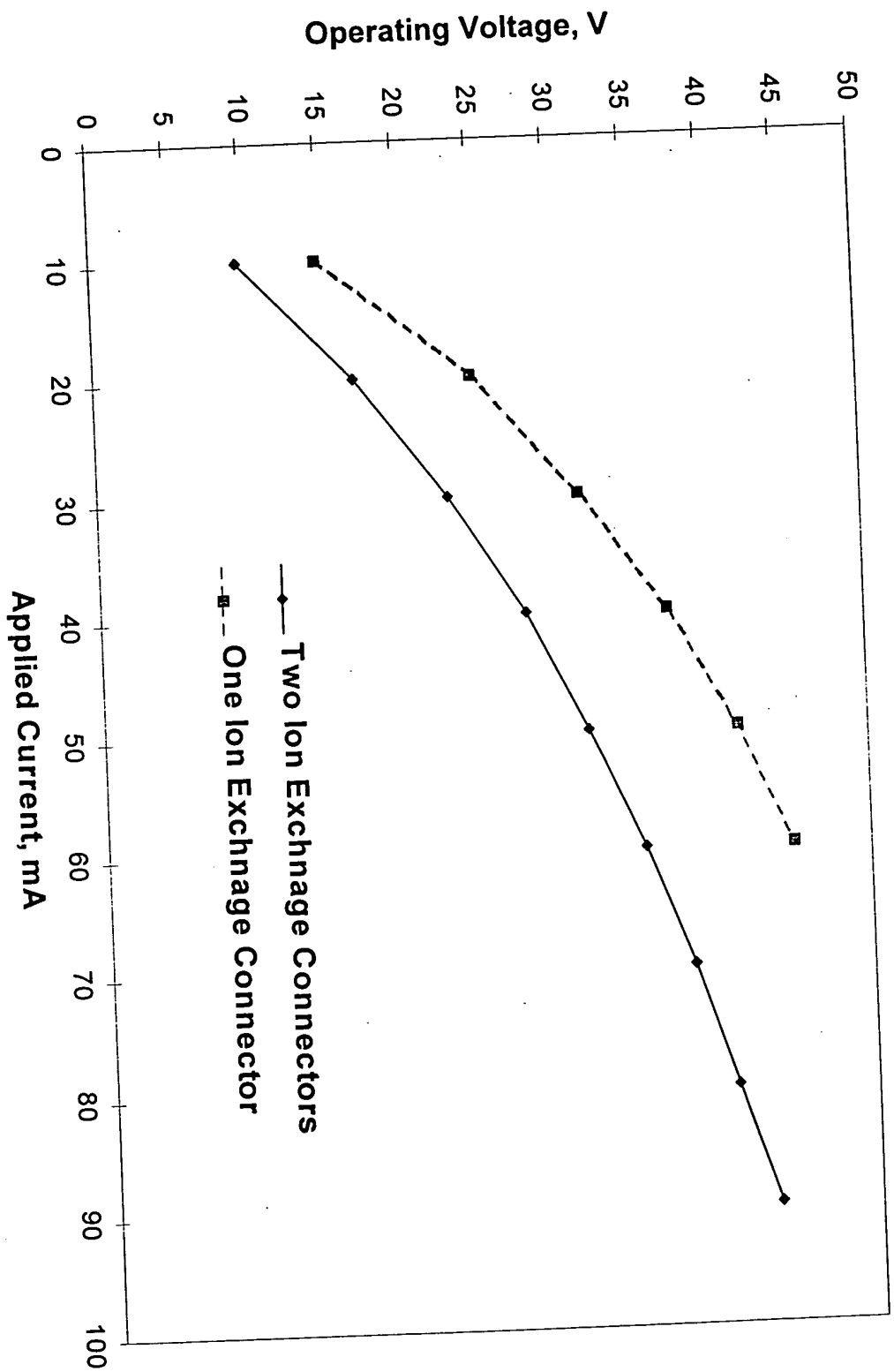


Figure 17

Operating Voltage (V) vs. Applied Current (mA) for Two Ion Exchange Connectors and One Ion Exchange Connector.

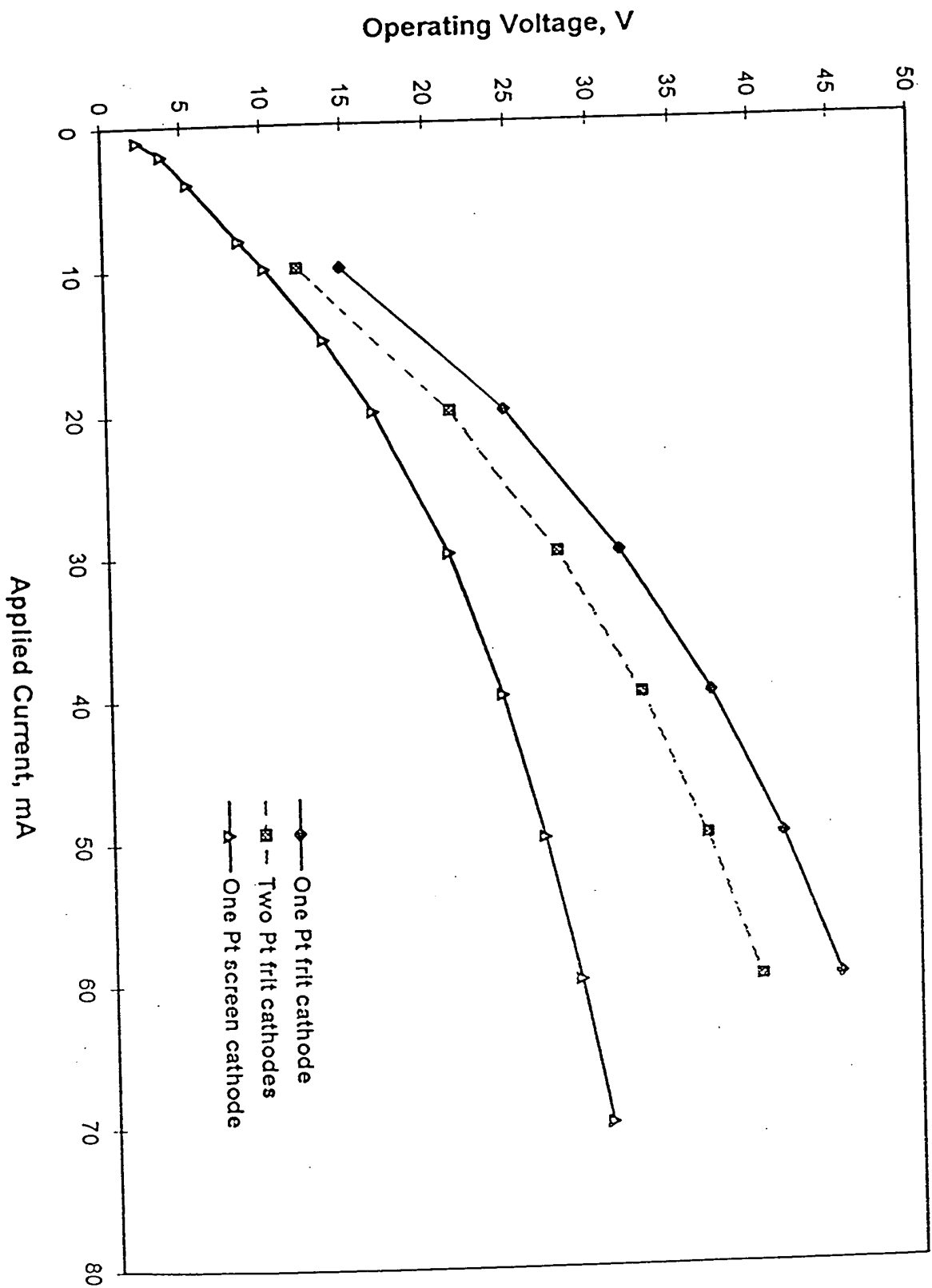
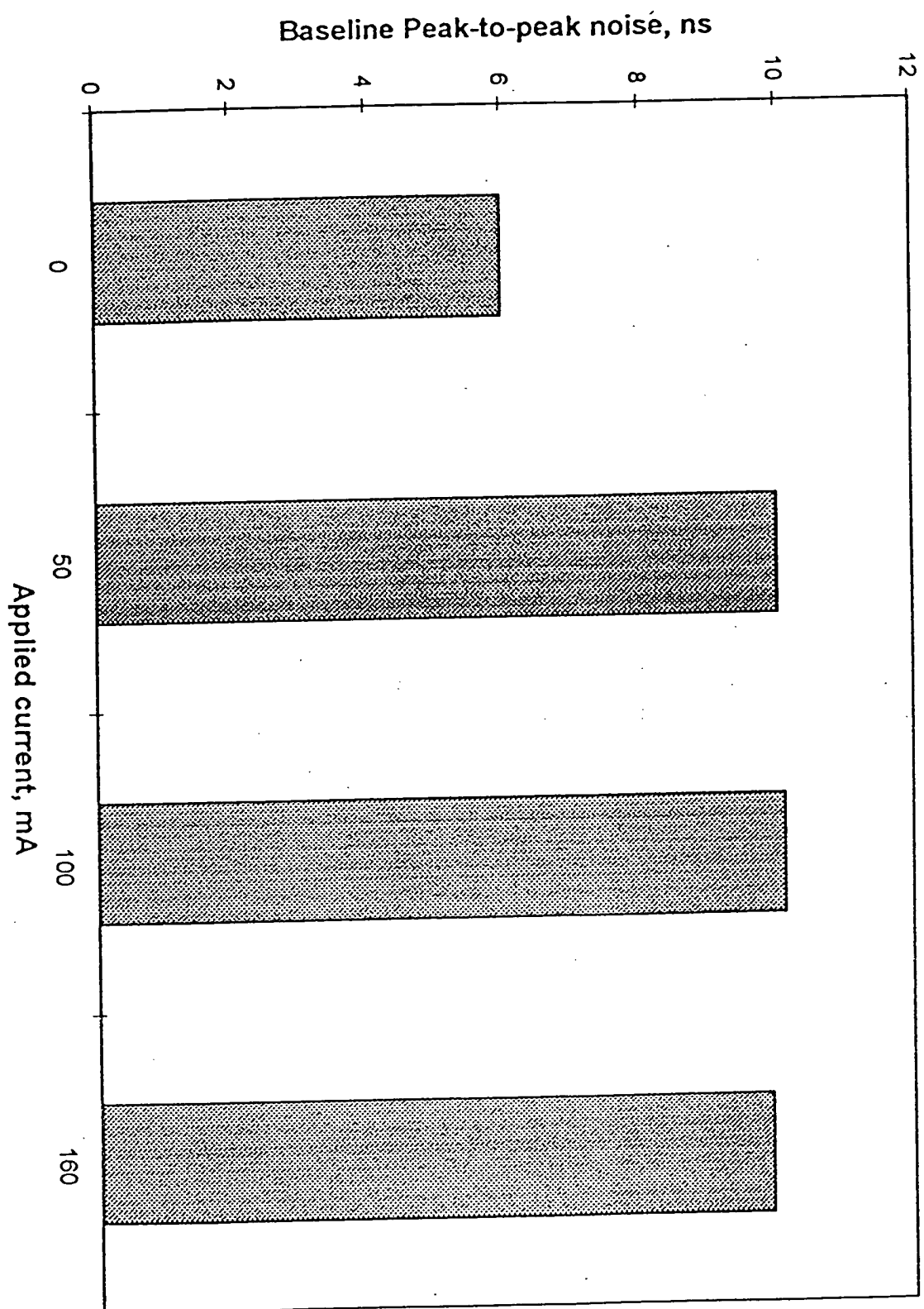


Figure 18

THESE DATA WERE OBTAINED FROM A STUDY OF THE EFFECT OF CATHODE CONFIGURATION ON THE OPERATING VOLTAGE OF A MERCURY-THALLIUM CELL.



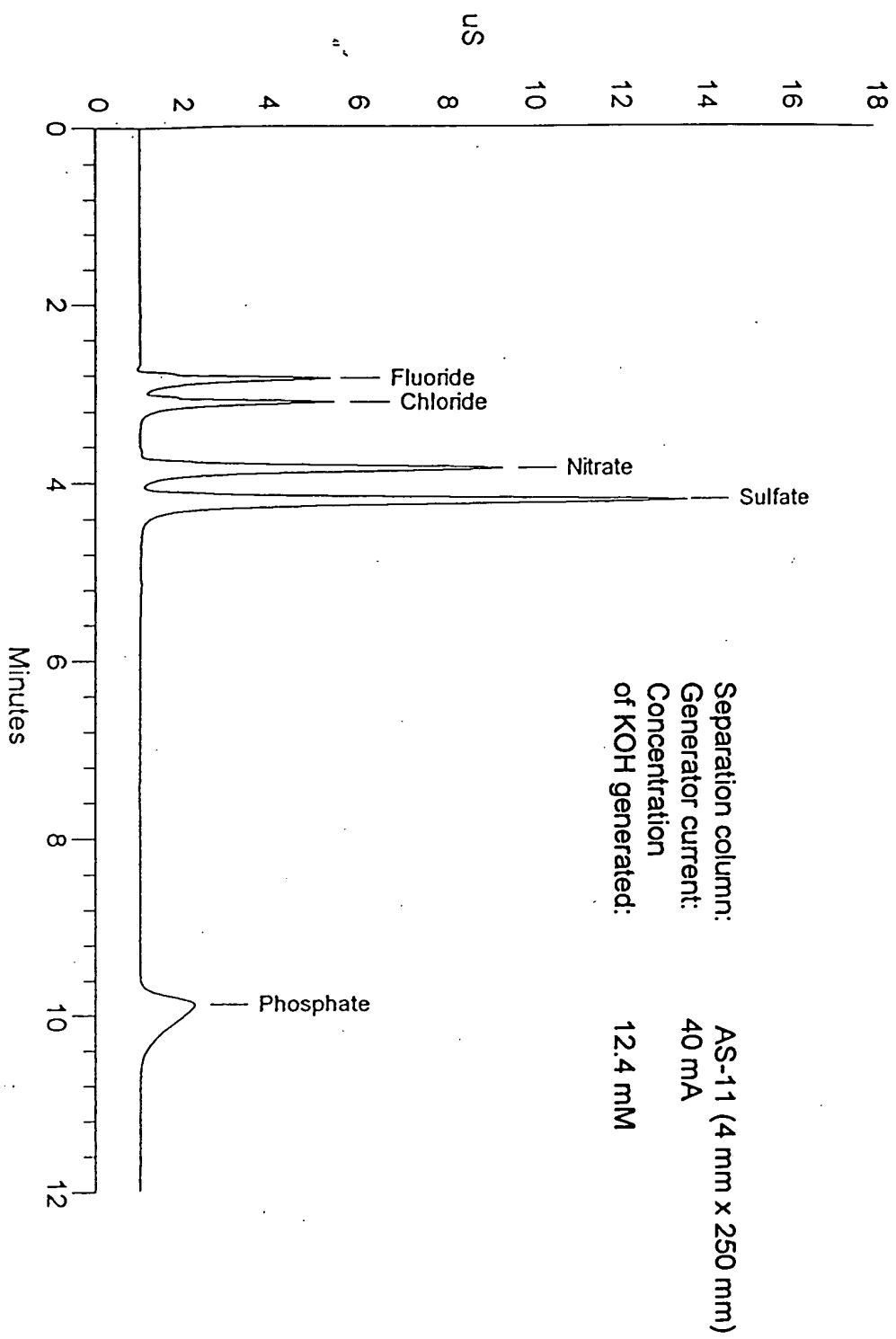


Figure 20.

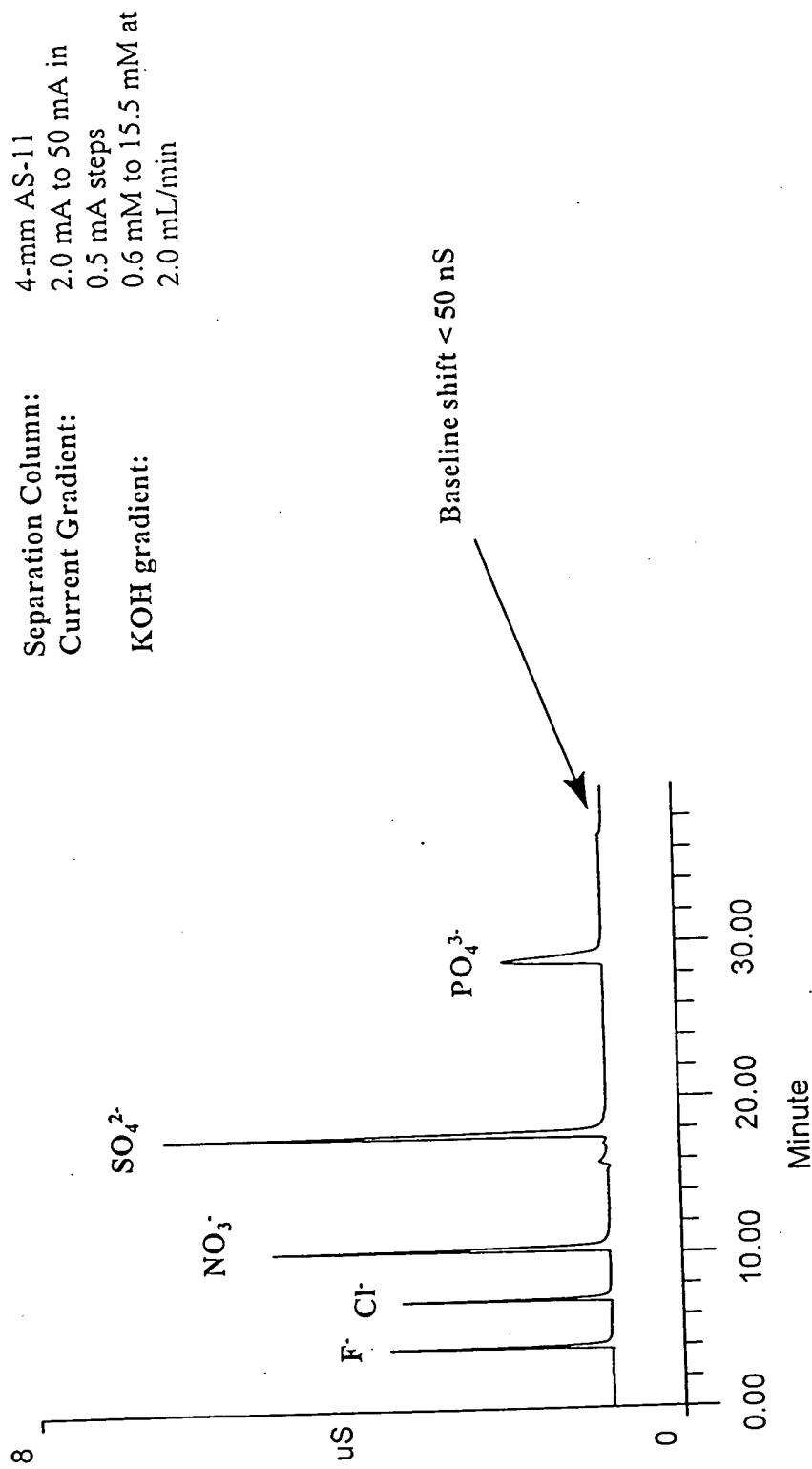


Figure 21.

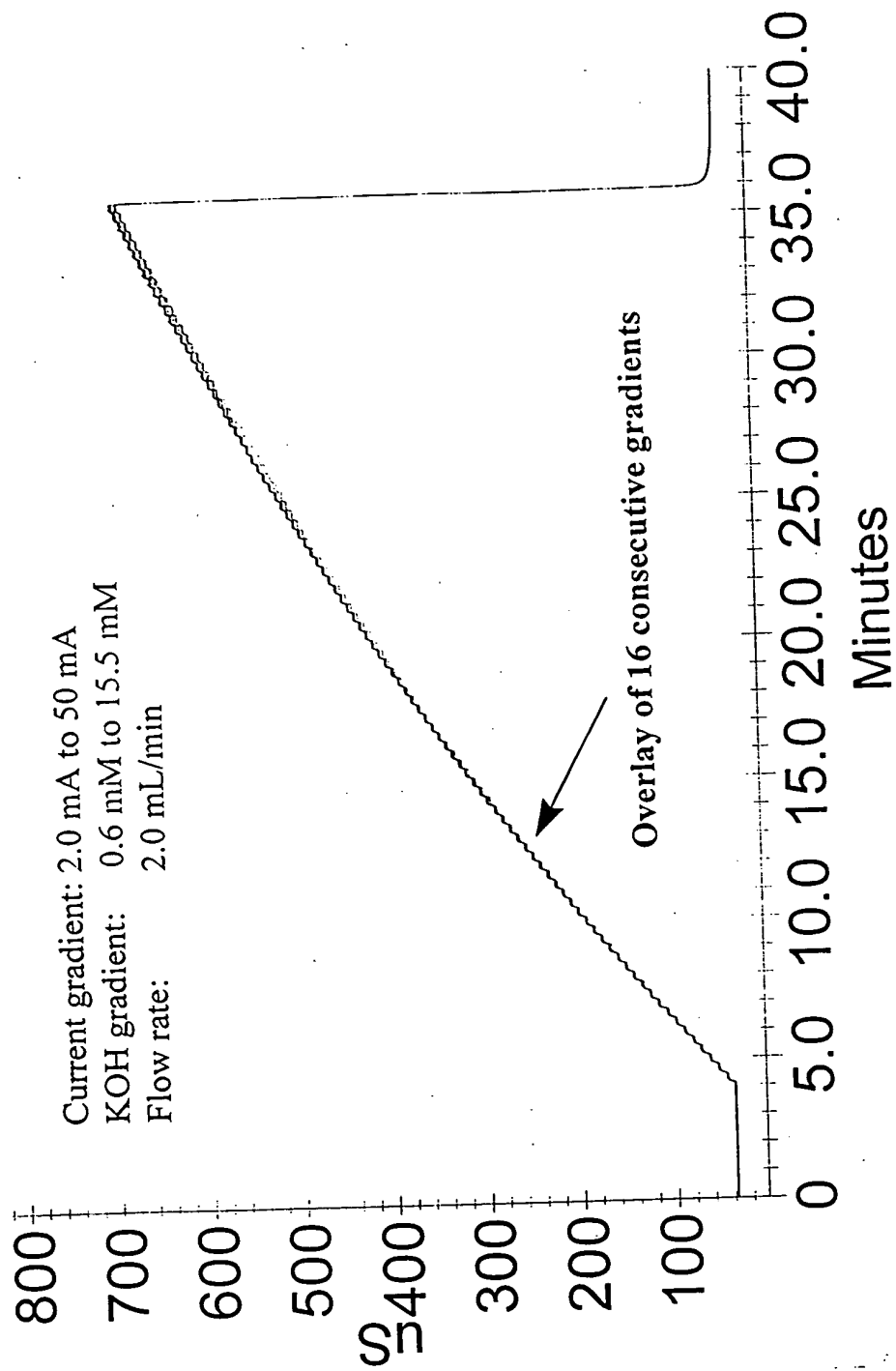


Figure 22.

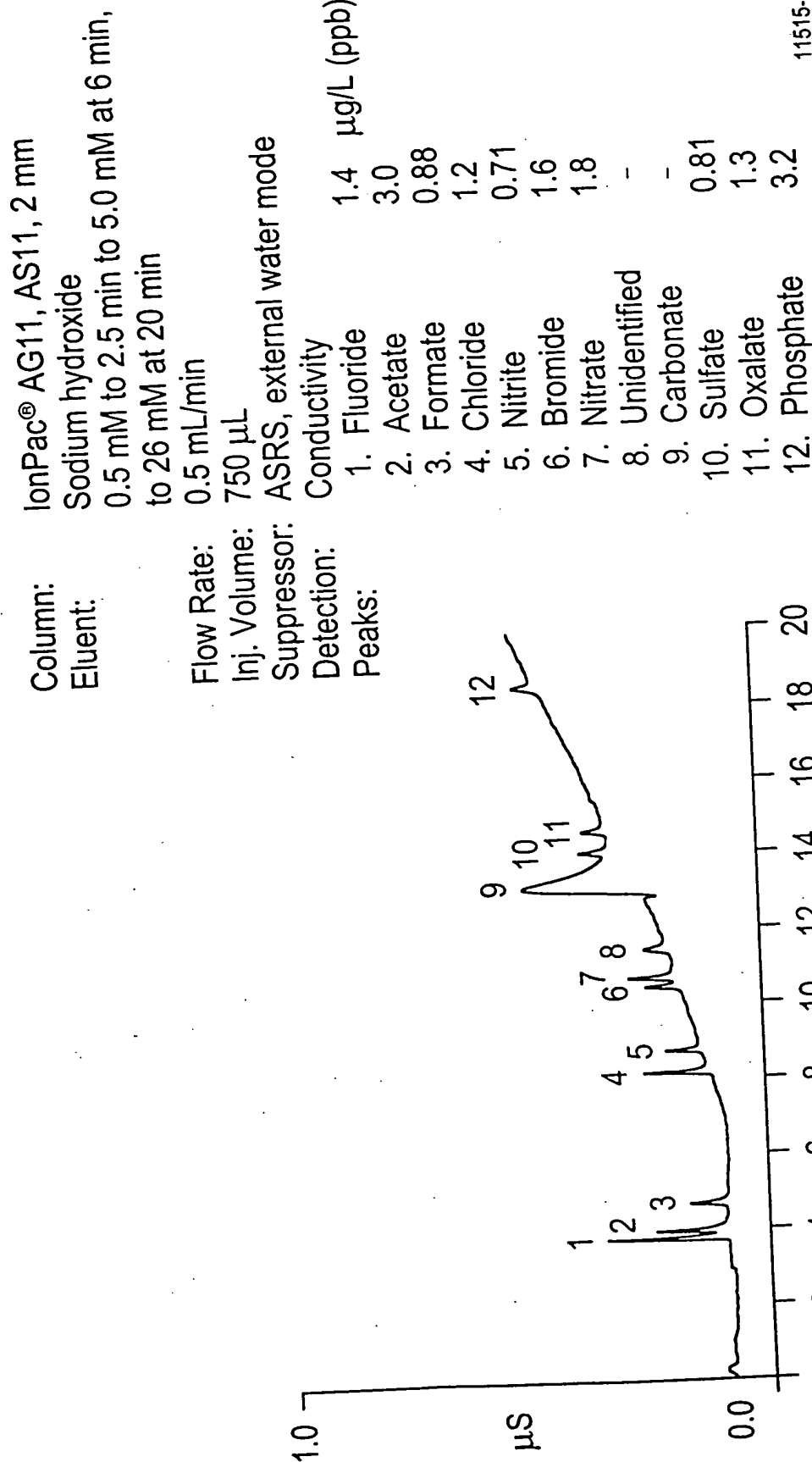


Figure 23.

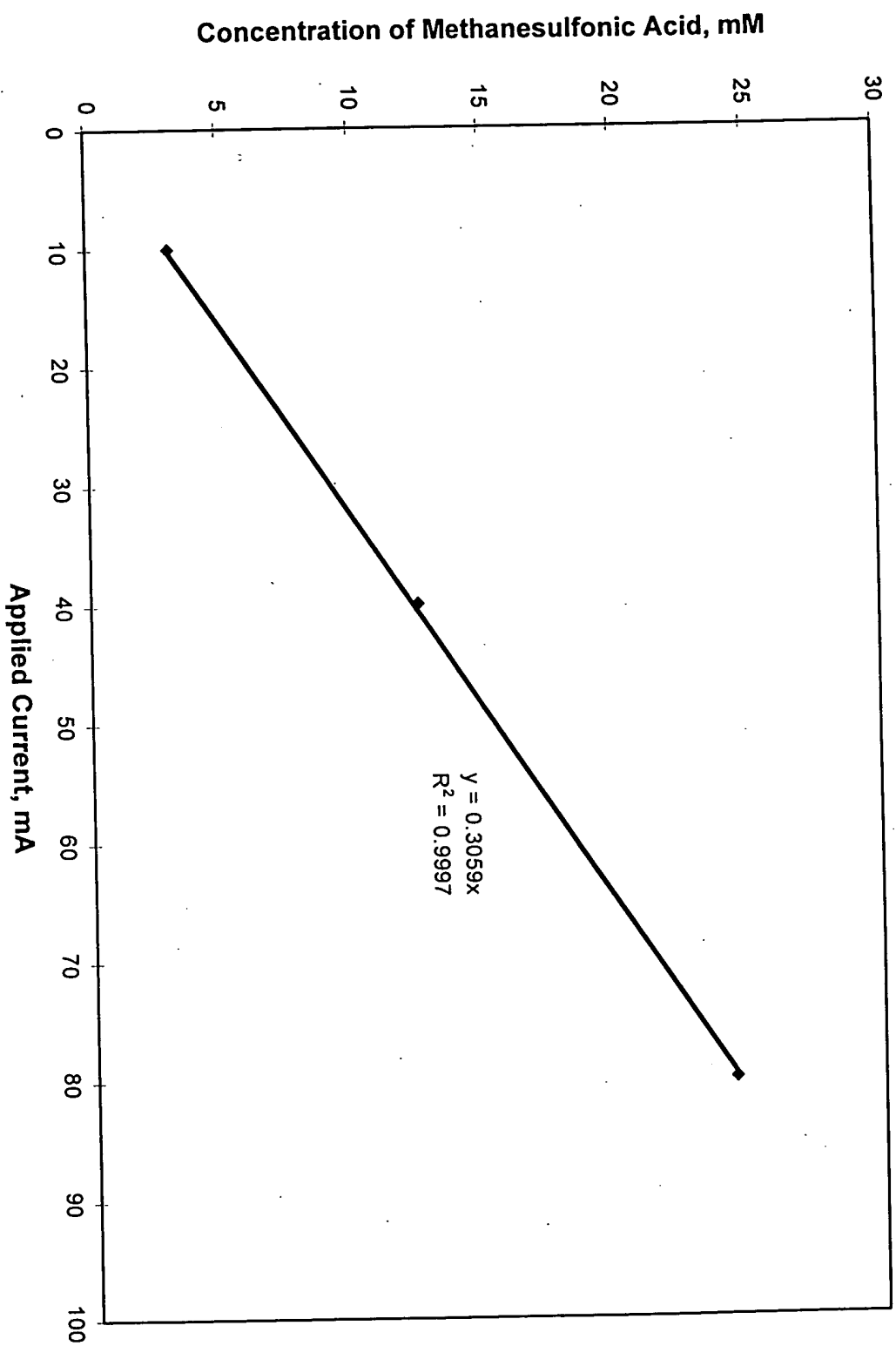


Figure 25.

Current gradient: 28.5 mA to 70 MA
MSA concentration: 17.7 mM to 43.5 mM
Flow rate: 1.0 mL/min

Overlay of 16 consecutive gradients

Minutes

Figure 26

CS12a (4 mm x250 mm)
17.7 mM to 43.5 mM MSA
28.5 mA to 70 mA
1.0 mL/min
750 uL

Column:
Eluent:
Current:
Flow rate:
inj. Volume:

Peak:
1. Lithium 5.0 ppb
2. Sodium 20
3. Ammonium 40
4. Potassium 20
5. Rubidium 100
6. Cesium 100
7. Magnesium 20
8. Calcium 100
9. Strontium 100
10. Barium 150

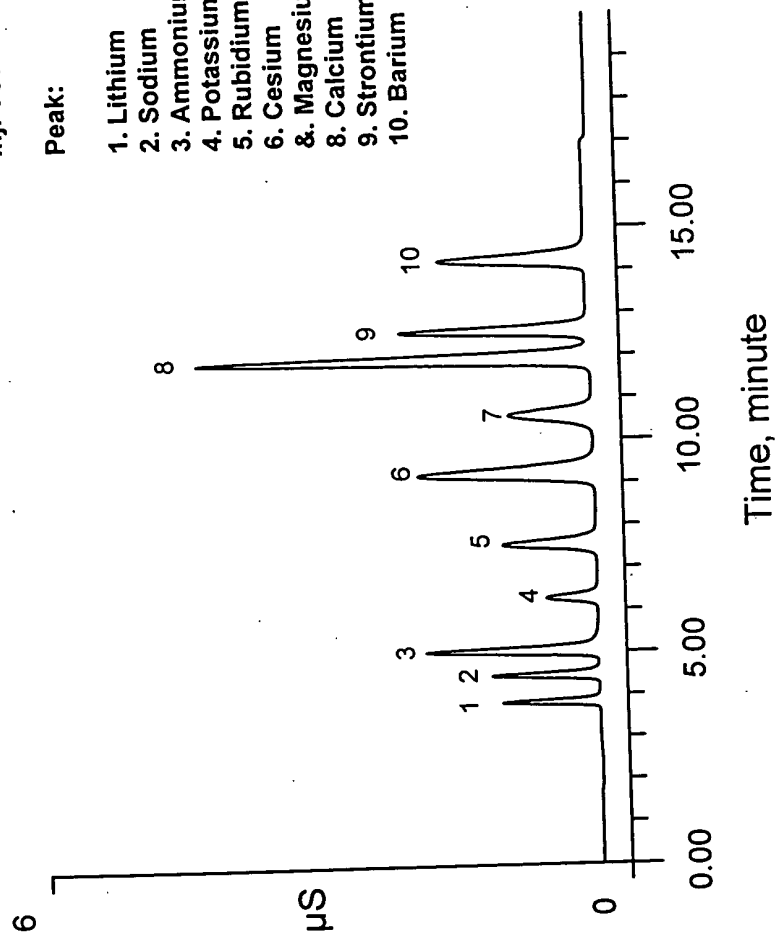


Figure 27.

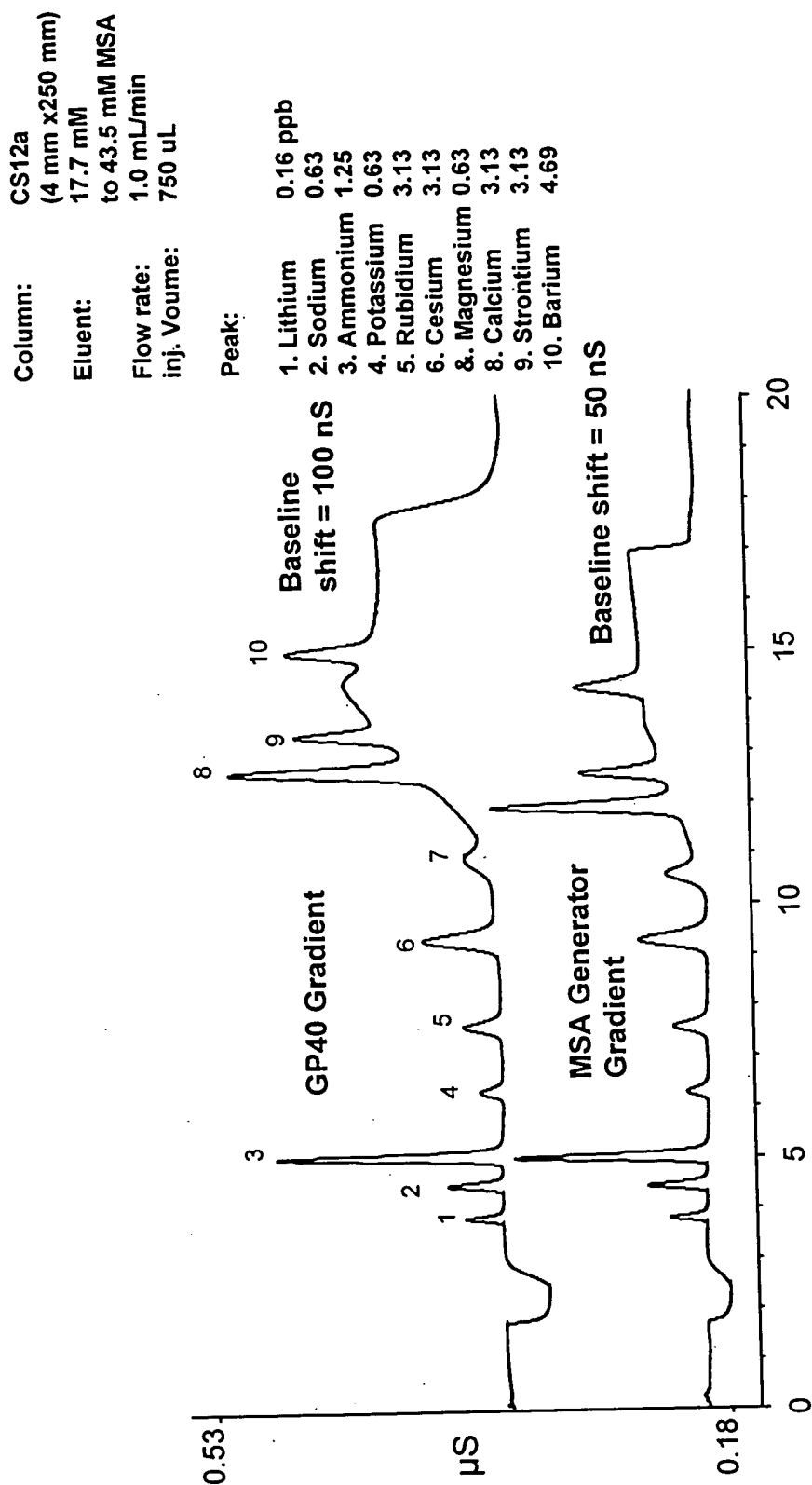


Figure 28.

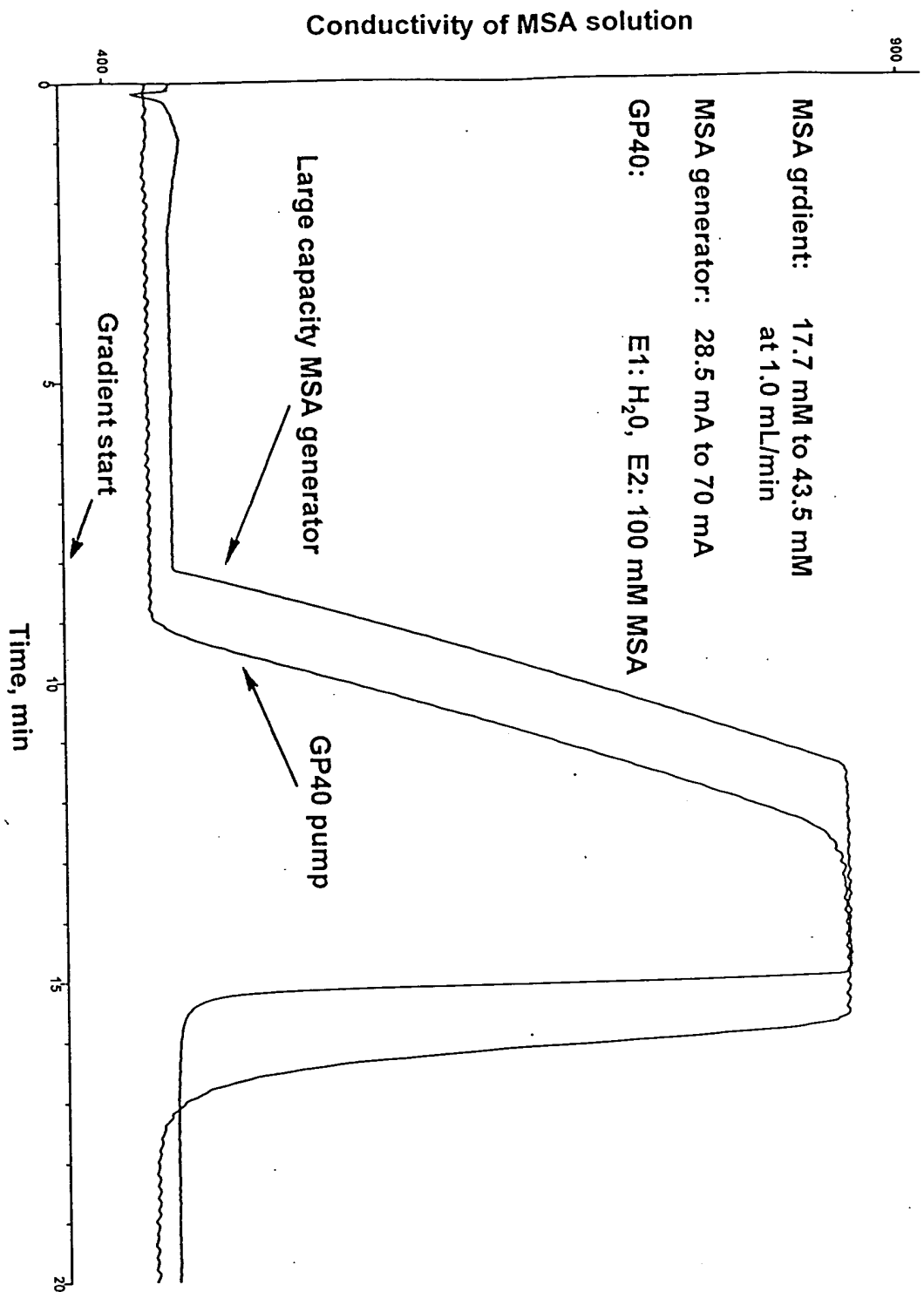


Figure 29.